

BRIEF COMMUNICATION

ON SOO'S EQUATIONS IN MULTIDOMAIN MULTIPHASE FLUID MECHANICS

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In a recent article, Sha & Soo (1978) present a set of equations for the general mixture conservation equations. The purpose of this note is to show that their model is not even valid in one-dimensional situations.

The general mixture conservation equation is presented by Sha & Soo as

$$\frac{\partial}{\partial t} \rho_m \psi_m + \nabla \cdot (\mathbf{U}_m \rho_m \psi_m) = -\nabla \cdot \mathbf{J}_m + \rho_m \phi_m. \quad [1]$$

Components of phases k relate to the mixture according to

$$\begin{aligned} \rho_m &= \sum_k \rho_k \\ \rho_m \mathbf{U}_m &= \sum_k \rho_k \mathbf{U}_k \\ \rho_m \psi_m &= \sum_k \rho_k \psi_k \\ \mathbf{J}_m &= \sum_k \mathbf{J}_{mk}. \end{aligned} \quad [2]$$

They thought that the basic conserved quantities, $\rho_m \psi_m$ are transferred with the velocity of the center-of-mass, \mathbf{U}_m across the surface of a control volume. Of course the mixture mass flux is transferred with \mathbf{U}_m across the surface of a control volume. But the mixture momentum and energy flux should be transferred with the velocity of the center-of-momentum, \mathbf{U}_p , and of the center-of-energy, \mathbf{U}_e , across the surface of a control volume, respectively. This concept is well illustrated by Lahey & Moody (1977). Here the velocity of the center-of-mass, \mathbf{U}_m in the two phase system is equivalent to the velocity of propagation of the plane through which no net mass flux passes. By equating the mass flux terms

$$\rho_G \alpha (U_G - U_m) = \rho_L (1 - \alpha) (U_m - U_L)$$

which produces

$$U_m = \frac{\rho_L U_L (1 - \alpha) + \rho_G U_G \alpha}{\rho_L (1 - \alpha) + \rho_G \alpha} = \frac{G}{\bar{\rho}} \quad [3]$$

where

$$\begin{aligned} G &= \rho_L U_L (1 - \alpha) + \rho_G U_G \alpha \\ \bar{\rho} &= \rho_L (1 - \alpha) + \rho_G \alpha. \end{aligned}$$

Similarly, by equating the momentum flux terms to define the plane through which zero net momentum flux passes,

$$\rho_G \alpha U_G (U_G - U_p) = \rho_L (1 - \alpha) U_L (U_p - U_L)$$

which produces

$$U_p = \frac{\rho_G \alpha U_G^2 + \rho_L (1 - \alpha) U_L^2}{\rho_G \alpha U_G + \rho_L (1 - \alpha) U_L} = \frac{G}{\rho'}, \quad [4]$$

where

$$\frac{1}{\rho'} = \frac{(1 - x)^2}{\rho_L (1 - \alpha)} + \frac{x^2}{\rho_G \alpha}.$$

Finally, by defining the plane through which no net energy flux passes

$$\rho_G \alpha e_G (U_G - U_e) = \rho_L (1 - \alpha) e_L (U_e - U_L)$$

which yields

$$U_e = \frac{\rho_G \alpha e_G U_G + \rho_L (1 - \alpha) e_L U_L}{\rho_G \alpha e_G + \rho_L (1 - \alpha) e_L} = \frac{Ge}{\bar{e}\bar{\rho}}, \quad [5]$$

where

$$e = e_L + x e_{LG}$$

and

$$\bar{e} = [\rho_G \alpha e_G + \rho_L (1 - \alpha) e_L] / \bar{\rho}.$$

Therefore U_m should be replaced by U_p for the momentum equations and by U_e for the energy equations. It is easy to prove this relationship

$$\frac{\partial}{\partial t} \rho_m \psi_m + \nabla \cdot (\mathbf{U}_i \rho_m \psi_m) = \frac{\partial}{\partial t} [\rho_L (1 - d) \psi_L + \rho_G \alpha \psi_G] + \nabla \cdot [\rho_L (1 - \alpha) U_L \psi_L + \rho_G \alpha U_G \psi_G], \quad [6]$$

where $U_i = U_m$ for the continuity equations; $U_i = U_p$ for the momentum equations; $U_i = U_e$ for the energy equations.

Now let us consider the conditions in which Sha & Soo's model is valid. Sha & Soo's model considers that $U_m = U_p = U_e$. In order to satisfy the above conditions $\bar{\rho}$ is equal to ρ' from [3] and [4].

$$\frac{\bar{\rho}}{\rho'} = 1 = [(1 - \alpha) \rho_L + \alpha \rho_G] \left[\frac{(1 - x)^2}{\rho_L (1 - \alpha)} + \frac{x^2}{\rho_G \alpha} \right] = \left[\frac{(1 - x)S + x}{U_L S (1 - x) + U_G x} \right] \left[\frac{U_L (1 - x)^2}{(1 - \alpha)} + \frac{U_G x^2}{\alpha} \right]. \quad [7]$$

If $\alpha = x$ and slip ratio, $S = 1$, [7] is satisfied. By $\alpha - x$ relation,

$$\alpha = \frac{x}{x + S \left(\frac{\rho_G}{\rho_L} \right) (1 - x)} \quad [8]$$

ρ_G should be equal to ρ_L in order to satisfy the above conditions, $\alpha = x$ and $S = 1$. The above result comes out of their postulate that the conservation equations for the mixture of a

multiphase system assume the same form as those for a homogeneous medium. It is clear that a multiphase system is different from a homogeneous medium such as an air system.

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